

A Numerical Analysis of Fluid Flow and Heat Transfer Characteristics of ZnO-Ethylene Glycol Nanofluid in Rectangular Microchannels

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The fluid flow and heat transfer characteristics of ZnO-Ethylene glycol (EG) nanofluid through rectangular microchannels having different aspect ratios (α is 1 to 2) are numerically investigated. The different nanoparticle volume percentages (φ is 1 % to 4 %) of ZnO-EG nanofluid are used. The flow is considered under single-phase, three-dimensional, steady-state, incompressible, thermally developing, laminar flow conditions. As a result, the microchannel with an aspect ratio value of 1 has the highest convection heat transfer coefficient and the lowest pressure drop. It is also observed that the convection heat transfer coefficient and pressure drop increases with an increase in nanoparticle volume fraction value of nanofluid. However, the Nusselt number decreases with increasing nanoparticle volume fraction, while the Darcy friction factor is not affected.

Keywords: convection heat transfer, pressure drop, rectangular microchannel, ZnO-EG nanofluid

Highlights

- ZnO-EG nanofluid flow and convective heat transfer characteristics through rectangular microchannels are numerically investigated.
- Thermal and hydrodynamic performances of rectangular microchannels are performed for different aspect ratios.
- Results showed that the thermal and hydrodynamic performances decrease with an increase in the aspect ratio of the rectangular microchannel.
- The Nusselt number decreases with increase in nanoparticle volume fraction of ZnO-EG nanofluid, while the Darcy friction factor is not affected.

0 INTRODUCTION

Nanofluids are prepared with the addition of nano-sized metallic or non-metallic particles to conventional working fluids to enhance their heat transfer ability. The term “nanofluid” was introduced by Choi [1] in 1995. In recent decades, the use of nanofluids as a heat transfer fluid in microchannel applications which are used in electronic device cooling has been investigated.

Azizi et al. [2] investigated the thermal performance of Cu-water nanofluid through a rectangular microchannel assembled into a cylindrical geometry. The Nusselt number is enhanced up to 23 % for 0.3 wt % nanoparticle addition. Rimbault et al. [3] reported that the CuO-water nanofluid flow through rectangular microchannels has the higher pressure drop by 70 % with a 4.5 % nanoparticle addition. However, the ratio of the amount of heat transferred to the pumping power required decreases with an increase in nanoparticle volume fraction. Kalteh [4] has compared different nanofluids which are a combination of nine different nanoparticle and three different base fluids. The highest and the lowest heat transfer coefficients were obtained for diamond-water and SiO₂-water nanofluid, respectively. However, the

obtained pressure drop values for all nanofluid type in same base fluid were almost equal. Halefadi et al. [5] have investigated fluid flow and heat transfer characteristics of CNT-water nanofluid through the rectangular microchannel. It was found that the nanofluid use reduces the total thermal resistance. Zhang et al. [6] have studied the fluid flow and heat transfer characteristics of Al₂O₃-water nanofluid through circular microchannels. The Nusselt number increased with increase in nanoparticle volume fraction and the Reynolds number. The maximum heat transfer enhancement was reported to be 10.6 %, while the Darcy friction factor increased by 7.9 %. Nebbati and Kadja [7] found that γ -Al₂O₃-water nanofluid use in microchannels increased the local Nusselt number and decreased the bottom surface temperature and shear stress on the wall.

Mohammed et al. [8] numerically studied the fluid flow and heat transfer characteristics of Al₂O₃-water nanofluid having different nanoparticle volume fractions through a rectangular microchannel. It was found that the heat transfer coefficient and wall shear stresses increase with increasing nanoparticle volume fraction, while thermal resistance decreases. Mohammed et al. [9] numerically compared the nanofluids prepared with the addition of Al₂O₃, Ag,

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CuO, diamond, SiO₂ and TiO₂ to water. The highest and the lowest heat transfer coefficients were obtained for the diamond-water and the Al₂O₃-water nanofluids, respectively. Moreover, the highest and the lowest pressure drops were obtained for SiO₂-water and Ag-water nanofluids, respectively. Salman et al. [10] compared the thermal performances of Al₂O₃-water and SiO₂-water nanofluid flows through microtubes, numerically and experimentally. They found that SiO₂-water nanofluid has the highest Nusselt number value and followed by Al₂O₃-water nanofluid and pure water, respectively. Mohammed et al. [11] numerically compared the thermal performances of Al₂O₃-water, Ag-water, SiO₂-water and TiO₂-water nanofluids through a square microchannel heat exchanger. The highest heat transfer coefficient was obtained for Al₂O₃-water nanofluid. Moreover, the lowest pressure drop was obtained for Ag-water nanofluid.

The thermophysical properties of working fluid are critical parameters of the thermal performance of working fluid, because the thermal performance parameters such as heat transfer rate, thermal diffusion, the Prandtl number, and the Reynolds number are related to thermophysical properties of working fluid. Therefore, the definition of thermophysical properties of nanofluids is a critical topic in the investigation of the thermal performance of nanofluids. Vajjha and Das [12] proposed a correlation to calculate the specific heat of nanofluids. In their study, Al₂O₃-EG/water (60:40), ZnO-EG/water (60:40), SiO₂-EG/water (60:40) nanofluids were used. They reported that the nanoparticle addition to base fluid decreased the specific heat of base fluid. Satti et al. [13] measured the specific heat of five different nanofluids containing Al₂O₃, ZnO, CuO, TiO₂, and SiO₂ nanoparticles dispersed in a base fluid of 60 % propylene glycol and 40% water by mass. It was found that the specific heat decreases with increase in nanoparticle volume fraction. At 243 K, specific heats of ZnO-PG/water (60:40) nanofluids for 0.5 % and 4.0 % nanoparticle addition reduce by about 28 % and 32 %, respectively. Esfe and Saedodin [14] and [15] proposed correlations to determine the thermal conductivity and viscosity of ZnO-EG nanofluids. Yu et al. [16] found that in low volume concentrations of ZnO-EG nanofluid showed Newtonian behavior, while at higher volume concentrations it showed shear-thinning behavior. Prajapati et al. [17] reported that the heat transfer coefficient increases with an increase in nanoparticle volume fraction of the ZnO-water nanofluid. Salman et al. [18] found that the highest Nusselt number was obtained for SiO₂-EG nanofluid, followed by ZnO-EG, CuO-EG, Al₂O₃-EG and pure EG.

EG and EG/water mixtures are used in car engines, heating systems, and solar heating installations as heat transfer fluids in cold regions. Nanofluid-based EG and EG/water mixtures can be used as alternative heat transfer fluids in these fields. Therefore, the fluid flow and heat transfer characteristics of nanofluid-based EG should clearly be investigated. From the above literature survey, it was clearly seen that the studies performed on the fluid flow and heat transfer characteristics of ZnO-EG nanofluid in microchannels are limited. In this study, the fluid flow and heat transfer characteristics of ZnO-EG nanofluid for different nanoparticle volume fractions through rectangular microchannels having different aspect ratios were numerically investigated under laminar flow conditions to investigate the use of ZnO-EG nanofluid as a heat transfer fluid in electronic device cooling and the importance of geometric configuration. The dimensionless temperatures, convective heat transfer coefficient, the Nusselt number, pressure drop, the Darcy friction factor values for ZnO-EG nanofluid were determined.

1 NUMERICAL PROCEDURE

1.1 Model Description

The system is considered to be a microchannel attached over a hot surface to dissipate heat generated by any electronic device (e.g. computer chips). The bottom wall of the microchannel is exposed to heat generated by the electronic device. The schematic diagram of the rectangular microchannel is illustrated in Fig. 1. Six different aspect ratios between α is 1 and 2 are defined. The hydraulic diameter and length of the microchannel for each aspect ratio values of the microchannel are assumed 150 μm and 5 cm, respectively. The other geometric parameters are defined by using the following equation,

$$D_h = \frac{4A}{P} = \frac{2HW}{(H+W)}, \quad (1)$$

where D_h , H and W are the hydraulic diameter, height and weight of microchannel, respectively.

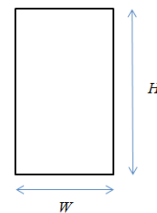


Fig. 1. The schematic diagram of microchannel

The obtained results for other geometric parameters belonging to the rectangular microchannel are shown in Table 1.

Table 1. The geometric dimensions of microchannels

$\alpha(H/W)$	$H [\mu\text{m}]$	$W [\mu\text{m}]$
1.0	150	150
1.2	165	137.5
1.4	180	128.57
1.6	195	121.875
1.8	210	116.67
2.0	225	112.5

1.2 Governing Equations

Fluid flow containing infinitesimal solid particles with diameters less than 100 nm can be modeled as single-phase flow [19]. Therefore, the ZnO-EG nanofluid flow is modelled as single-phase flow in this study. The following assumptions are also adopted for this study: (i) both heat transfer and fluid flow in microchannel are in three dimensional and steady-state; (ii) nanofluid flow is incompressible and laminar; (iii) the physical properties of nanofluid, such as density, specific heat, thermal conductivity are temperature independent; and (iv) the buoyancy effect, viscous dissipation and radiation heat transfer are negligible. The governing equations for the single-phase model can be written as follows under the abovementioned assumptions:

Continuity equation:

$$\frac{\partial U}{\partial X} + \frac{\partial V}{\partial Y} + \frac{\partial W}{\partial Z} = 0, \quad (2)$$

X-momentum equation:

$$\left(U \frac{\partial U}{\partial X} + V \frac{\partial U}{\partial Y} + W \frac{\partial U}{\partial Z} \right) = -\frac{dP}{dX} + \frac{1}{Re} \left(\frac{\partial^2 U}{\partial X^2} + \frac{\partial^2 U}{\partial Y^2} + \frac{\partial^2 U}{\partial Z^2} \right), \quad (3)$$

Y-momentum equation:

$$\left(U \frac{\partial V}{\partial X} + V \frac{\partial V}{\partial Y} + W \frac{\partial V}{\partial Z} \right) = -\frac{dP}{dY} + \frac{1}{Re} \left(\frac{\partial^2 V}{\partial X^2} + \frac{\partial^2 V}{\partial Y^2} + \frac{\partial^2 V}{\partial Z^2} \right), \quad (4)$$

Z-momentum equation:

$$\left(U \frac{\partial W}{\partial X} + V \frac{\partial W}{\partial Y} + W \frac{\partial W}{\partial Z} \right) = -\frac{dP}{dZ} + \frac{1}{Re} \left(\frac{\partial^2 W}{\partial X^2} + \frac{\partial^2 W}{\partial Y^2} + \frac{\partial^2 W}{\partial Z^2} \right), \quad (5)$$

Energy equation:

$$\left(U \frac{\partial \theta}{\partial X} + V \frac{\partial \theta}{\partial Y} + W \frac{\partial \theta}{\partial Z} \right) = \frac{1}{Re \cdot Pr} \left(\frac{\partial^2 \theta}{\partial X^2} + \frac{\partial^2 \theta}{\partial Y^2} + \frac{\partial^2 \theta}{\partial Z^2} \right), \quad (6)$$

where X , Y , and Z are dimensionless distances; U , V , and W are the dimensionless velocity components; Re is the Reynolds number; Pr is the Prandtl number; P is the dimensionless pressure and θ is the dimensionless temperature.

The dimensionless parameters in the above equations can be expressed as follows:

$$X = \frac{x}{D_h}, \quad Y = \frac{y}{D_h}, \quad Z = \frac{z}{D_h}, \quad (7)$$

$$U = \frac{u}{U_{in}}, \quad V = \frac{v}{U_{in}}, \quad W = \frac{w}{U_{in}}, \quad (8)$$

$$Re = \frac{\rho U_{in} D_h}{\mu}, \quad (9)$$

$$Pr = \frac{C_p \mu}{k}, \quad (10)$$

$$P = \frac{\Delta P}{\rho U_{in}^2}, \quad (11)$$

$$\theta = \frac{T - T_m}{T_w - T_m}, \quad (12)$$

where u , v , w are the velocity components in x , y and z coordinates; ρ is the density; μ is the viscosity; C_p is the specific heat; k is the thermal conductivity; ΔP is the pressure drop; U_{in} is the inlet velocity; T_w and T_{in} are the wall and inlet temperature, respectively.

To solve the governing equations, boundary conditions are required. The inlet velocity is obtained by considering the Reynolds numbers. The no-slip condition is imposed at the walls of the microchannel. The fixed heat flux is applied at the bottom surface of the microchannel, and the heat is transferred from the bottom wall to the nanofluid. The side and top surfaces of the microchannel are assumed to be insulated. The pressure outlet boundary condition is used at the outlet of the microchannel. The boundary conditions used in this study are given below in detail:

at the inlet: $U = 1, \theta = 1,$

at the outlet: $P = P_{out} = 0,$

at the solid-fluid interfaces:

$$U = 0, \theta = \theta_s, -k \frac{\partial \theta}{\partial n} = -k_s \frac{\partial \theta_s}{\partial n},$$

at the bottom surface: $q_w'' = -k_s \frac{\partial \theta_s}{\partial n},$

at the side and top surfaces: $q_w'' = 0.$

1.3 Thermophysical Properties

The governing equations include some thermophysical properties belonging to working fluid. To solve the governing equations, these thermophysical properties should be defined.

The density and specific heat of the ZnO-EG nanofluid can be determined using the following equations, which are based on conventional mixture theory, respectively:

$$\rho_{nf} = (1 - \varphi) \rho_{bf} + \varphi \rho_{np}, \quad (13)$$

$$(\rho C_p)_{nf} = (1 - \varphi) (\rho C_p)_{bf} + \varphi (\rho C_p)_{np}, \quad (14)$$

where φ is the nanoparticle volume fraction of the nanofluid and the subscripts nf , np and bf denote nanofluid, nanoparticle, and the base fluid, respectively.

To calculate the thermal conductivity of ZnO-EG nanofluid, the following correlation proposed by Esfe and Saedodin [14], which is based on experimental data obtained for ZnO-EG nanofluid can be used;

$$k_{nf} = \left(0.24859T^{2.504\varphi^{0.7974}} + 0.7492 \right) k_{bf}, \quad (15)$$

where T is the temperature and in units of °C. The validity of this correlation is in $\varphi = 0.0625\%$ to 5% and $T = 25\text{ °C}$ to 50 °C intervals.

The viscosity of ZnO-EG nanofluid can be calculated by using following correlation proposed by Esfe and Saedodin [15] which is based on experimental data obtained for ZnO-EG nanofluid;

$$\mu_{nf} = \left(\frac{0.9118 \text{Exp}(5.49\varphi - 0.00001359T^2) + 0.0303 \text{Ln}(T)}{1} \right) \mu_{bf}, \quad (16)$$

where T is the temperature and in units of °C. This correlation is valid for $\varphi = 0.25\%$ to 5% and $T = 25\text{ °C}$ to 50 °C .

1.4 Numerical Procedure

To carry out the numerical computation, the finite volume method is used. The governing equations are solved along with boundary conditions. The convective terms existing in the governing equations are discretized by using the second order upwind scheme. The standard scheme is employed in the discretization of pressure. A SIMPLE algorithm is used to resolve the velocity and pressure coupling [20]. The SIMPLE-code family is based on the spatial integration of the conservation equations over finite control volumes. The Green-Gauss cell-based method is used to discretize the momentum and energy equations. The governing equations are iterated until the convergence value of 1×10^{-6} . No convergence problems are observed during the calculations.

1.5 Grid Testing and Validation

In the modelling of the rectangular microchannel, the hexahedral mesh distribution is used. Finer meshes are used in the region near the microchannel walls to enhance the accuracy of the solution. The mesh distribution of rectangular microchannel is shown in Fig. 2.

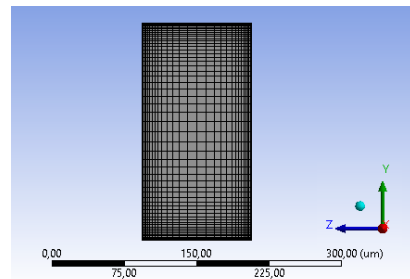


Fig. 2. The mesh distribution of rectangular microchannel

The grid independence test is realized for each microchannel with different aspect ratios to invalidate the effect of grid number on a solution. Six different grid numbers ranging from 40,000 to 1,400,000 are used to model each microchannel. Optimum grid numbers are defined considering the change of result obtained by the solution. The numerical computations are realized for defined optimum models.

To validate the accuracy of code, the results obtained by the present study are compared with the results of Lee et al. [21], which are based on experimental data for rectangular microchannels in thermally developing laminar flow under constant heat flux conditions. The comparison of the results obtained by the present study with that of Lee et al.

[21] is illustrated in Fig. 3. As can be seen, the local Nusselt number values obtained by the present study showed good agreement with the results of Lee et al. [21]. The maximum deviation from the results of Lee et al. [21] is obtained to be 9.45 %.

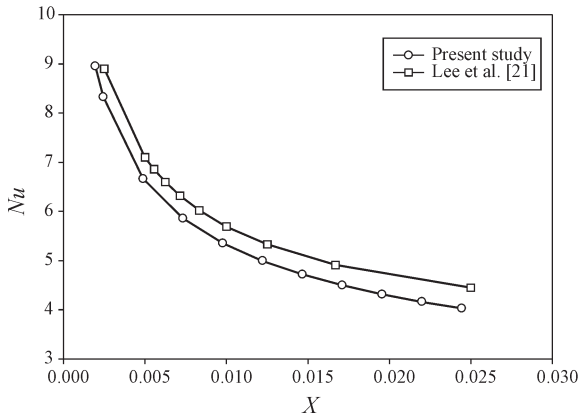


Fig. 3. Comparison of results obtained by present study with the results of Lee et al. [21]

2 RESULTS AND DISCUSSION

The fluid flow and heat transfer characteristics of ZnO-EG nanofluid through rectangular microchannels are numerically investigated. In the calculations, different nanoparticle volume fractions ($\varphi=1\%$ to 4%) of ZnO-EG nanofluid are used. The Reynolds number is in the range of 10 to 100. The calculations are realized for different aspect ratio values ($\alpha=1, 1.2, 1.4, 1.6, 1.8, 2$) of the rectangular microchannel. The fixed heat flux of 1000 W/m^2 is applied at the bottom surface of the microchannels.

2.1 Dimensionless Temperature

The dimensionless temperature is calculated by using Eq. (12). The variation of dimensionless temperature along with axial dimensionless distance for each aspect's ratio values of the rectangular microchannel in the use of pure EG at $Re = 10$ and $Re = 100$ are illustrated in Figs. 4a and b, respectively.

The variation of the dimensionless temperature along with the axial dimensionless distance for different nanoparticle volume fractions in $\alpha=1$ at $Re=10$ and $Re=100$ are illustrated in Figs. 5a and b, respectively.

The ZnO nanoparticle addition to pure EG decreased the bulk and wall temperature of the fluid. However, the decrease in wall temperature is higher than that of the bulk temperature. Therefore, the

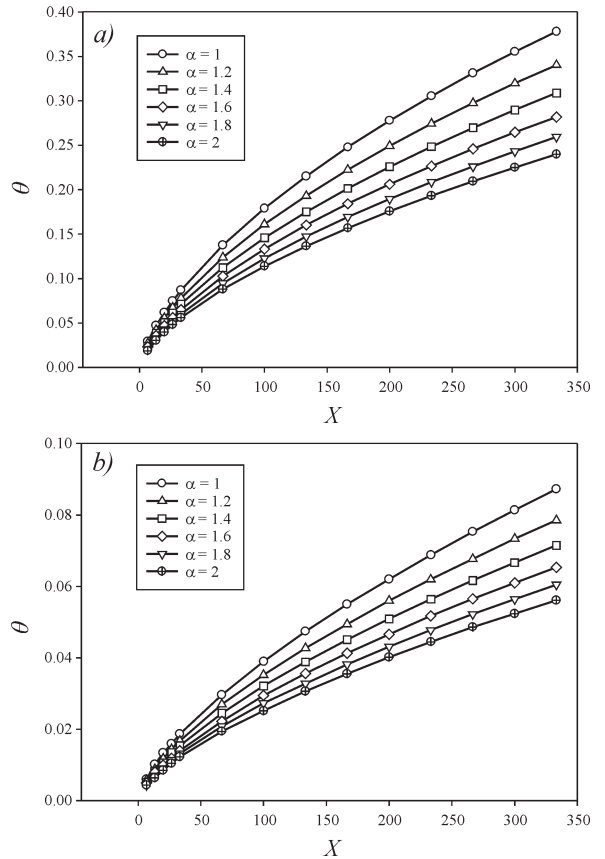


Fig. 4. The variation of dimensionless temperature along with axial dimensionless distance for different aspect ratios (working fluid is pure EG) at a) $Re = 10$ and b) $Re = 100$

dimensionless temperature increases with an increase in the nanoparticle volume fraction of ZnO nanofluid.

2.2 Convective Heat Transfer Coefficient

The convective heat transfer coefficient can be written as follows:

$$h = \frac{\dot{m}C_p(T_{outlet} - T_{inlet})}{A_s(T_w - T_b)}, \quad (17)$$

where \dot{m} is the mass flow rate, and A_s is the heated surface area of the microchannel.

The variation of convective heat transfer coefficient with the Reynolds number for each aspect ratio of the rectangular microchannel in the use of pure EG is illustrated in Fig. 6.

As can be seen from Fig. 6, the convective heat transfer coefficient decreases with an increase in aspect ratio of the rectangular microchannel. The convective heat transfer coefficients obtained for $\alpha=1$

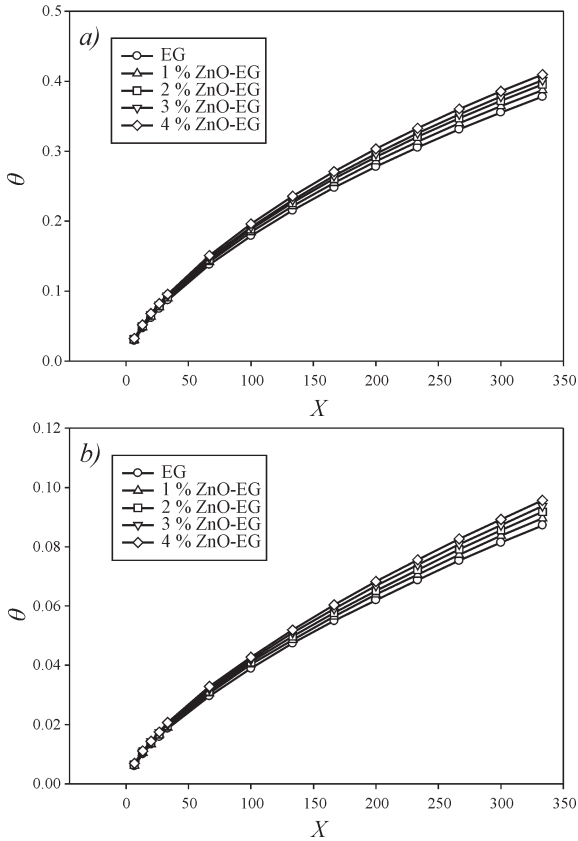


Fig. 5. The variation of dimensionless temperature along with axial dimensionless distance for different nanoparticle volume fractions (for $\alpha = 1$) at a) $Re = 10$ and b) $Re = 100$

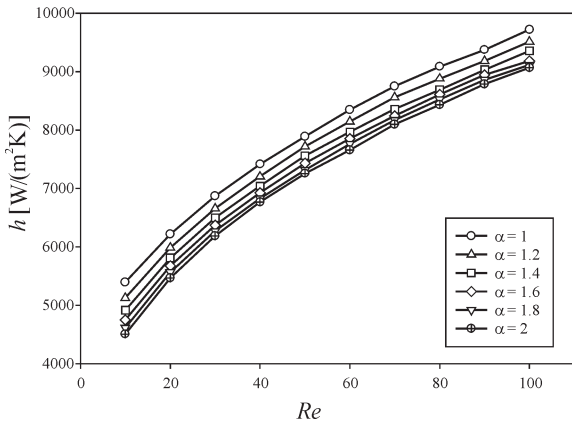


Fig. 6. The variation of convective heat transfer coefficient with the Reynolds number for different aspect ratios (working fluid is pure EG)

at $Re = 10$ and $Re = 100$ is higher by 19.69 % and 7.18 % compared to that of $\alpha = 2.0$, respectively. The microchannel having an aspect ratio of $\alpha = 1$ provides better heat dissipation by convection heat transfer. The microchannel width is decreased with increasing

aspect ratio to be able to provide constant hydraulic diameter. This tendency causes decreases in the heated surface area of the microchannel and consequently increases the convective heat transfer coefficient. However, a decrease in the outlet temperature of pure EG with increasing aspect ratio is higher than the decrease in heated surface area. Therefore, the convective heat transfer coefficient decreases with the increasing aspect ratio of the microchannel.

The variation of convective heat transfer coefficient with the Reynolds number for different nanoparticle volume fractions in $\alpha=1$ is illustrated in Fig. 7.

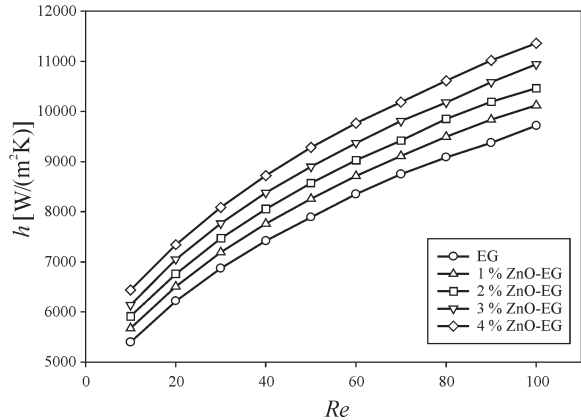


Fig. 7. The variation of convective heat transfer coefficient with the Reynolds number for different nanoparticle volume fractions (for $\alpha=1$)

The convective heat transfer coefficient increases with the increase in nanoparticle volume fraction of ZnO-EG nanofluid. The increments in the convective heat transfer coefficient for 4 % ZnO-EG nanofluid compared to pure EG is 19.33 % and 16.89 % at $Re = 10$ and $Re = 100$, respectively. The ZnO nanoparticle addition to pure EG increases the density, outlet temperature of the nanofluid, and the velocity of the nanofluid at fixed Reynolds numbers. Moreover, the ZnO nanoparticle addition to pure EG decreases the temperature difference between wall and bulk temperatures of nanofluid. This fact is also reported by Tsai and Chein [22]. These facts increase the convective heat transfer coefficient of flow. The specific heat of pure EG decreases with increasing nanoparticle volume fraction. This case has a reducing effect on the convective heat transfer coefficient but is eliminated by other additive effects.

The variation of local convective heat transfer coefficient along with axial dimensionless distance for each aspect ratio of the rectangular microchannel

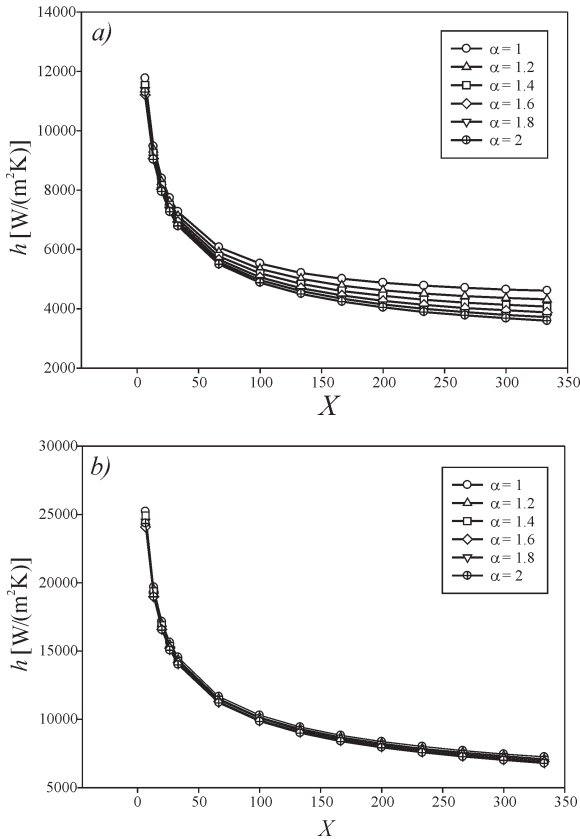


Fig. 8. The variation of local convective heat transfer coefficient along with axial dimensionless distance for different aspect ratios (working fluid is pure EG) at a) $Re = 10$ and b) $Re = 100$

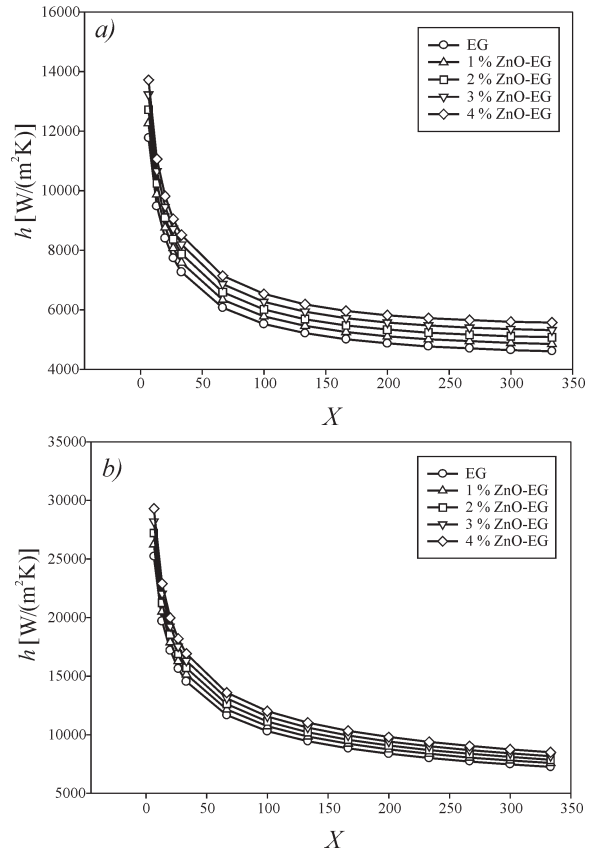


Fig. 9. The variation of local convective heat transfer coefficient along with axial dimensionless distance for different nanoparticle volume fractions ($\alpha = 1$) at a) $Re = 10$ and b) $Re = 100$

in the use of pure EG at $Re = 10$ and $Re = 100$ are illustrated in Figs. 8a and b, respectively.

As can be seen from Figs 8a and b, the local convective heat transfer values are much higher in the inlet region of the microchannel. It is also observed that the reduction in local convective heat transfer coefficient after the inlet region of the microchannel at $Re = 100$ is higher compared to that of at $Re = 10$.

The variation of local convective heat transfer coefficient along with the axial dimensionless distance for different nanoparticle volume fractions in $\alpha = 1$ at $Re = 10$ and $Re = 100$ are illustrated in Figs. 9a and b, respectively.

As expected, the local convective heat transfer coefficients for 4 % ZnO-EG nanofluid take higher values in comparison to other nanoparticle volume fractions of ZnO-EG nanofluid and pure EG. It is also observed that the ZnO-EG nanofluid flow is thermally developing a flow for this study.

2.3 The Nusselt Number

The Nusselt number is expressed as follows:

$$Nu = \frac{hD_h}{k} \tag{18}$$

The variation of the Nusselt number with the Reynolds number for each aspect ratio of the rectangular microchannel in the use of pure EG is illustrated in Fig. 10.

The Nusselt number decreases with increases in the aspect ratio of the rectangular microchannel. It is found that the Nusselt number obtained for $\alpha=1$ at $Re=10$ and $Re=100$ is higher by 19.69 % and 7.18 % compared to that of $\alpha=2$, respectively.

The variation of the Nusselt number with the Reynolds number for different nanoparticle volume fractions in $\alpha=1$ is illustrated in Fig. 11.

As can be seen from Fig. 11, the Nusselt number surprisingly decreases with increases in nanoparticle

volume fraction of ZnO-EG nanofluid. The Nusselt number values for 4.0 % ZnO-EG nanofluid at $Re=10$ and $Re=100$ are lower by 2.02 % and 4.02 % compared to that of pure EG, respectively.

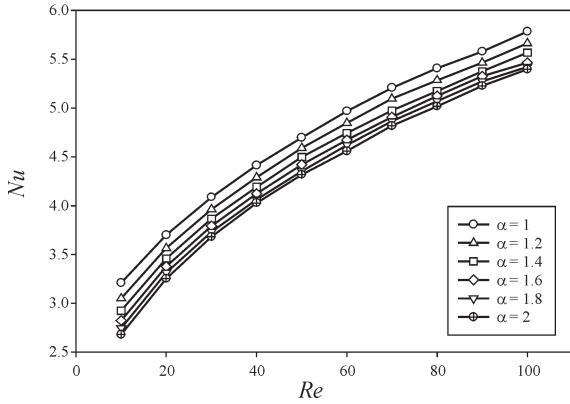


Fig. 10. The variation of the Nusselt number with the Reynolds number for different aspect ratios (working fluid is pure EG)

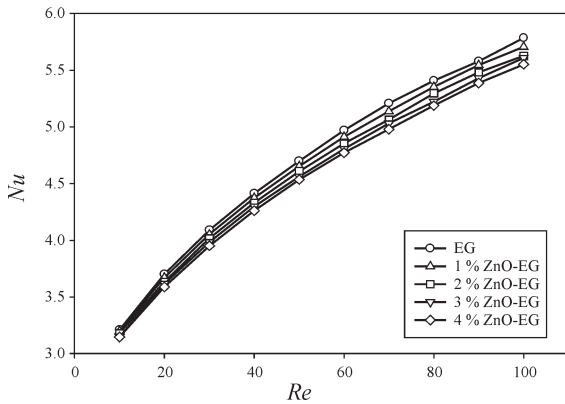


Fig. 11. The variation of the Nusselt number with the Reynolds number for different nanoparticle volume fractions (for $\alpha = 1$)

The reason for the decrease in the Nusselt number is a higher increment in conductive heat transfer coefficient when ZnO nanoparticle is added to pure EG. The increment in convective heat transfer coefficient is obtained to be 19.33 % for 4 % ZnO-EG nanofluid at $Re=10$, while the increment in conductive heat transfer coefficient is 21.78 % for 4 % ZnO-EG nanofluid. This higher increment in conductive heat transfer coefficient compared to convective heat transfer coefficient reduces the Nusselt number of the flow.

2.4 Pressure Drop

The variation of normalized pressure drop with the Reynolds number for each aspect ratio of the

rectangular microchannel in the use of pure EG is illustrated in Fig. 12.

The normalized pressure drop increases with increases in aspect ratio of the rectangular microchannel. It is found that the normalized pressure drop for $\alpha=2$ at $Re = 10$ and $Re = 100$ is 9.05 % and 8.91 % higher compared to that of $\alpha=1$, respectively.

The variation of normalized pressure drop with the Reynolds number for different nanoparticle volume fractions in $\alpha=1$ is illustrated in Fig. 13, respectively.

It is found that the normalized pressure drop increases with increases in nanoparticle volume fraction of ZnO-EG nanofluid in that ZnO nanoparticle addition to pure EG increases the viscosity of the nanofluid. The normalized pressure drop values for 4 % ZnO-EG nanofluid at $Re = 10$ and $Re = 100$ are 28.96 % and 29.23 % higher compared to that of pure EG, respectively.

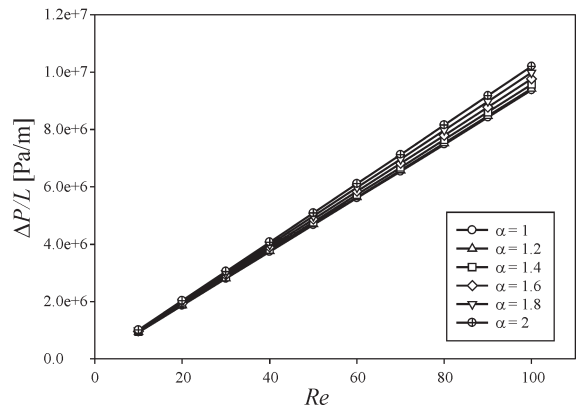


Fig. 12. The variation of normalized pressure drop with the Reynolds number for different aspect ratios (working fluid is pure EG)

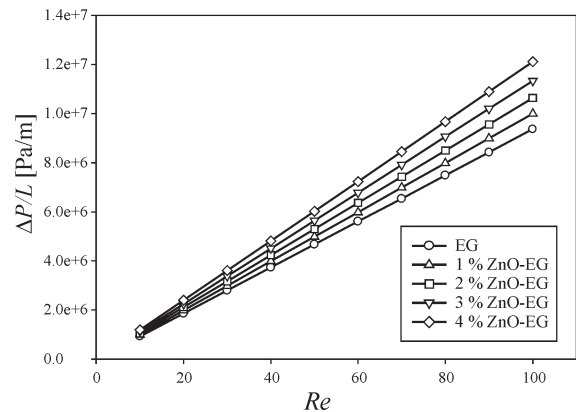


Fig. 13. The variation of normalized pressure drop with the Reynolds number for different nanoparticle volume fractions (for $\alpha = 1$)

2.5 The Darcy Friction Factor

The Darcy friction factor is determined as follows:

$$f = 2 \frac{D_h}{L} \frac{\Delta P}{\rho U_{in}^2}, \quad (19)$$

where L is the length of the microchannel, ΔP is the pressure drop.

The variation of the Darcy friction factor with the Reynolds number for each aspect ratio of the rectangular microchannel in the use of pure EG is illustrated in Fig. 14.

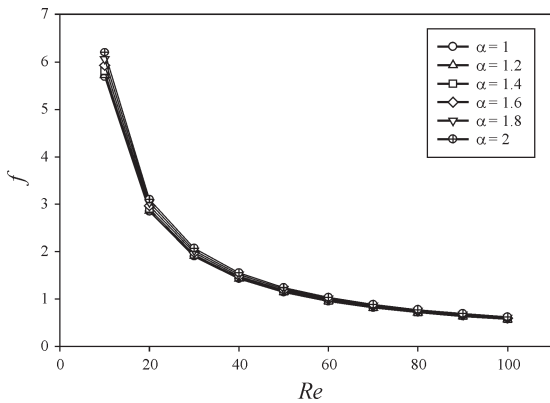


Fig. 14. The variation of the Darcy friction factor with the Reynolds number for different aspect ratios (working fluid is pure EG)

The Darcy friction factor increases with increases in the aspect ratio of the rectangular microchannel. The pressure drop for $\alpha=2$ at $Re = 10$ and $Re = 100$ is 9.05 % and 8.91 % higher compared to that of $\alpha=1$, respectively.

The variation of the Darcy friction factor with the Reynolds number for different nanoparticle volume fractions in $\alpha=1$ is illustrated in Fig. 15.

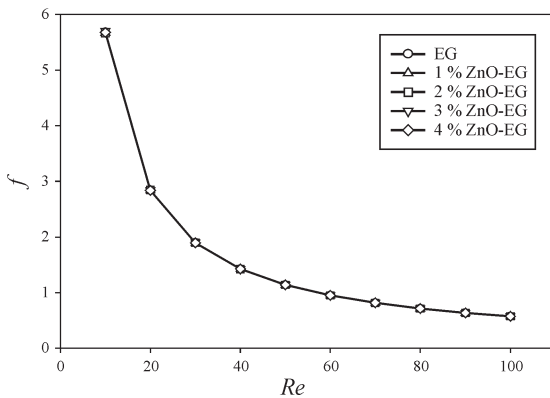


Fig. 15. The variation of the Darcy friction factor with the Reynolds number for different nanoparticle volume fractions (for $\alpha = 1$)

It is observed that the ZnO nanoparticle addition to pure EG does not affect the Darcy friction factor. The same finding is reported for Al_2O_3 -water and Al_2O_3 -EG/water nanofluids by Jung et al. [23].

The local Darcy friction factor can be calculated as follows

$$f_x = \frac{8\tau_x}{\rho U_{in}^2}, \quad (20)$$

where τ_x is local shear stress.

The variation of the local Darcy friction factor along with axial dimensionless distance for each aspect ratio of the rectangular microchannel in the use of pure EG at $Re = 10$ and $Re = 100$ are illustrated in Figs. 16a and b, respectively.

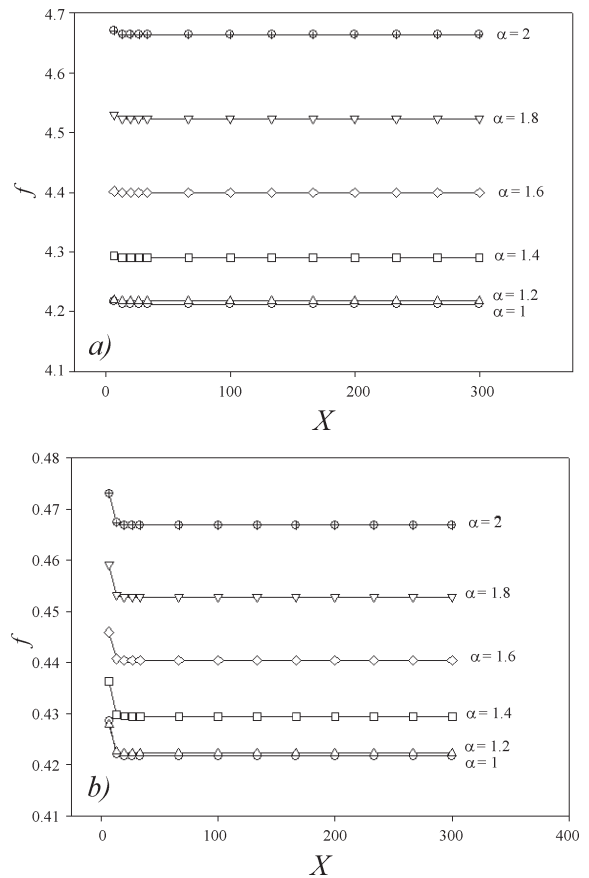


Fig. 16. The variation of the local Darcy friction factor along with axial dimensionless distance for different aspect ratios (working fluid is pure EG) at a) $Re=10$ and b) $Re=100$

As can be seen from Figs 16a and b, the flow is hydrodynamically developed. The velocity of flow and the local shear stress values increase with an increase in the Reynolds number. However, an increase in velocity is higher than that of local shear

stress. Therefore, the local Darcy friction values for $Re = 10$ are higher than that of $Re = 100$. The highest local Darcy friction factor values along with the axial dimensionless distance are obtained for $\alpha=2$, while the lowest values are obtained for $\alpha=1$. The surface area of a microchannel increases with increases in aspect ratio of the microchannel. A larger surface area leads to increases in local shear stress.

2.6 Thermal Resistance and Pumping Power

Thermal resistance can be defined as follows:

$$R_{th} = \frac{T_w - T_{in}}{Q_{in}}, \quad (21)$$

where Q_{in} is the amount of heat transferred to nanofluid.

Another important parameter is the pumping power required to drive the nanofluid through the microchannel. The pumping power required can be written as:

$$W = U_{in} A_c \Delta P, \quad (22)$$

where A_c is the cross-section area of the microchannel.

The increase in nanoparticle volume fraction of ZnO-EG nanofluid reduces the wall temperature. Therefore, the increase in the nanoparticle volume fraction of ZnO-EG nanofluid caused a reduction in thermal resistance.

The nanoparticle addition to working fluid also increases the pressure drop and, therefore, the pumping power increases. The nanofluids should be evaluated by their thermal resistance in a given pumping power.

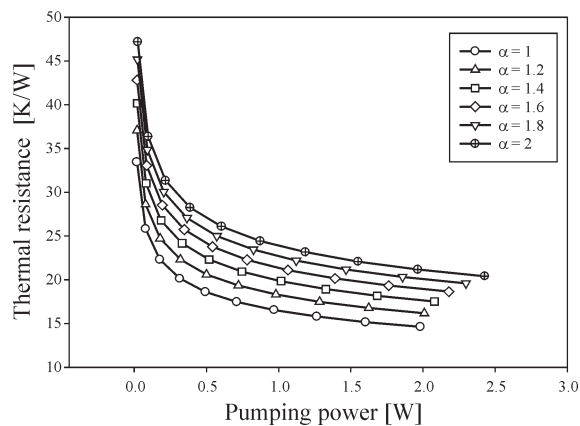


Fig. 17. The variation of thermal resistance with pumping power required for different aspect ratios (working fluid is pure EG)

The variation of the thermal resistance with pumping power required for each aspect ratios of the rectangular microchannel in the use of pure EG is illustrated in Fig. 17.

In a given pumping power required, the highest thermal resistance values are obtained for $\alpha=2$, while the lowest values are obtained for $\alpha=1$.

The variation of thermal resistance with pumping power required for different nanoparticle volume fractions of ZnO-EG nanofluid in $\alpha = 1$ is illustrated in Fig. 18.

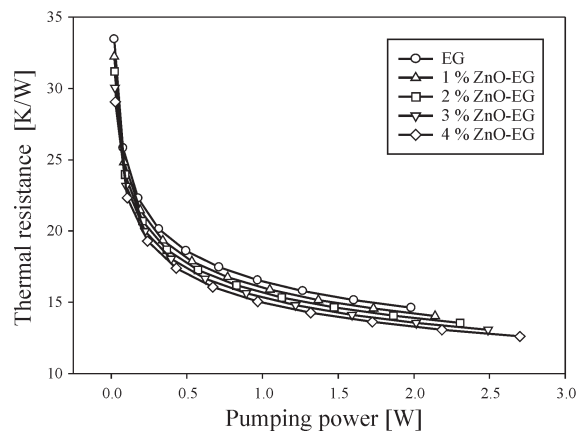


Fig. 18. The variation of thermal resistance with pumping power required for different aspect ratios (working fluid is pure EG)

In a given pumping power, the highest thermal resistance values are obtained for pure EG. The thermal resistance decreases with increases in the nanoparticle volume fraction of ZnO-EG nanofluid. The lowest thermal resistance values for a required pumping power are obtained for 4 % ZnO-EG nanofluid.

4 CONCLUSIONS

The fluid flow and heat transfer characteristics of ZnO-EG nanofluid through rectangular microchannels with different aspect ratios are numerically investigated. The results showed that the geometrical configuration of microchannels is a very effective parameter on fluid flow and heat transfer characteristics. Therefore, the hydrodynamic and thermal performances of microchannels can be enhanced with only geometric configuration in the system design. The microchannel with $\alpha=1$ gave better results in the sense of both fluid flow and heat transfer. In the analyses, the different nanoparticle volume fractions of ZnO-EG nanofluid are used as a working fluid. The use of ZnO-EG nanofluid enhanced the convection heat transfer;

however, it simultaneously increased the pressure drop. In this case, the thermal resistance value at a given pumping power provides insight about the advantage or disadvantage of nanofluid use. ZnO-EG nanofluid has an advantage over pure EG due to their lower thermal resistance values at a given pumping power compared to pure EG.

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